

The temperature of the gases in the furnace is 1800°F. The heat transfer coefficient on the inside of the furnace is 37 Btu/hr-ft<sup>2</sup>-°F, and the heat transfer coefficient for ambient air outside the furnace is 5 Btu/hr-ft<sup>2</sup>-°F. The ambient air temperature is 70°F. The overall heat transfer coefficient for the furnace is most nearly

- (A) 0.104 Btu/hr-ft<sup>2</sup>-°F
- (B) 0.213 Btu/hr-ft<sup>2</sup>-°F
- (C) 0.345 Btu/hr-ft<sup>2</sup>-°F
- (D) 0.467 Btu/hr-ft<sup>2</sup>-°F

#### Solution

The overall resistance to heat transfer per unit area is obtained by adding up the individual resistances per unit area. The overall heat transfer coefficient for the furnace is

$$\begin{aligned} \frac{1}{U} &= \frac{1}{h_i} + \left(\frac{t}{k}\right)_b + \left(\frac{t}{k}\right)_s + \left(\frac{t}{k}\right)_i + \frac{1}{h_o} \\ U &= \frac{1}{\frac{1}{h_i} + \left(\frac{t}{k}\right)_b + \left(\frac{t}{k}\right)_s + \left(\frac{t}{k}\right)_i + \frac{1}{h_o}} \\ &= \frac{1}{\frac{1}{37 \frac{\text{Btu}}{\text{hr-ft}^2\text{-}^\circ\text{F}}} + \frac{6 \text{ in}}{\left(0.41 \frac{\text{Btu}}{\text{hr-ft}^2\text{-}^\circ\text{F}}\right)\left(12 \frac{\text{in}}{\text{ft}}\right)} + \frac{2 \text{ in}}{\left(25 \frac{\text{Btu}}{\text{hr-ft}^2\text{-}^\circ\text{F}}\right)\left(12 \frac{\text{in}}{\text{ft}}\right)} + \frac{3 \text{ in}}{\left(0.03 \frac{\text{Btu}}{\text{hr-ft}^2\text{-}^\circ\text{F}}\right)\left(12 \frac{\text{in}}{\text{ft}}\right)} + \frac{1}{\left(5 \frac{\text{Btu}}{\text{hr-ft}^2\text{-}^\circ\text{F}}\right)\left(12 \frac{\text{in}}{\text{ft}}\right)}} \\ &= 0.1041 \text{ Btu/hr-ft}^2\text{-}^\circ\text{F} \quad (0.104 \text{ Btu/hr-ft}^2\text{-}^\circ\text{F}) \end{aligned}$$

**The answer is (A).**

When conduction and convection (but not radiation) are the only modes of heat transfer, the *overall*

*coefficient of heat transfer*,  $U$ , also known as the *overall conductivity*, *overall heat transmittance*, or simply *U-factor*, is defined by Eq. 17.32.

$$\begin{aligned} U &= \frac{1}{AR_{\text{th,total}}} \\ &= \frac{1}{\sum_i \frac{L_i}{k_i} + \sum_j \frac{1}{h_j}} \end{aligned} \quad 17.32$$

The overall coefficient is usually used in conjunction with the outside (exposed) surface area (because it is easier to measure), but not always. Therefore, it will generally be written with a subscript (e.g.,  $U_o$  or  $U_i$ ) indicating which area it is based on. The heat transfer is

$$Q = U_o A_o (T_1 - T_2) = U_i A_i (T_1 - T_2) \quad 17.33$$

When heat transfer occurs by two or three modes, the overall coefficient of heat transfer takes all active modes—conduction, convection, and radiation—into consideration. In that sense, the overall coefficient,  $U$ , is defined by Eq. 17.34, rather than being used in it.

$$U = \frac{Q}{A(T_1 - T_2)} \quad 17.34$$

#### Example 17.4

A 100 ft<sup>2</sup> (9.3 m<sup>2</sup>) wall consists of 4 in (10 cm) of red brick ( $k = 0.38$  Btu-ft/hr-ft<sup>2</sup>-°F (0.66 W/m·K)), 1 in (2.5 cm) of pine ( $k = 0.06$  Btu-ft/hr-ft<sup>2</sup>-°F (0.10 W/m·K)), and ½ in (1.2 cm) of plasterboard ( $k = 0.30$  Btu-ft/hr-ft<sup>2</sup>-°F (0.52 W/m·K)). The internal and external film coefficients are 1.65 Btu/hr-ft<sup>2</sup>-°F and 6.00 Btu/hr-ft<sup>2</sup>-°F (9.38 W/m<sup>2</sup>-K and 34.1 W/m<sup>2</sup>-K), respectively. The inside and outside air temperatures are 72°F (22°C) and 30°F (−1°C), respectively. Determine the heat transfer.

#### SI Solution

Convert the thicknesses from centimeters to meters.

$$L_{\text{brick}} = \frac{10 \text{ cm}}{100 \frac{\text{cm}}{\text{m}}} = 0.10 \text{ m}$$

$$L_{\text{pine}} = \frac{2.5 \text{ cm}}{100 \frac{\text{cm}}{\text{m}}} = 0.025 \text{ m}$$

$$L_{\text{plasterboard}} = \frac{1.2 \text{ cm}}{100 \frac{\text{cm}}{\text{m}}} = 0.012 \text{ m}$$