

## Chapter 16, Problem 2

[Return to Questions \(/admin/questions/0?sfield=magento\\_id&stext=0000087567&sdka=&stype=&sdiff=\)](/admin/questions/0?sfield=magento_id&stext=0000087567&sdka=&stype=&sdiff=)

# Test Bank

 Question preview

## Question

A turbine receives steam at a rate of 12 kg/s. At the outlet, the steam is at 200°C and 0.10 MPa (enthalpy of 2875.5 kJ/kg). At the inlet, the steam is at 250°C and 0.20 MPa (enthalpy of 2971.3 kJ/kg). In addition, the steam experiences an increase in kinetic energy of 1.92 kJ/kg. Assume the turbine is adiabatic. The fluid power extracted by the turbine is most nearly

## Answers

- (A) 200 kW
- (B) 350 kW
- (C) 1200 kW
- (D) 3500 kW

The answer is (C).

## Solution

Determine the fluid power imparted by the turbine.



$$\begin{aligned}
 \dot{W}_{\text{turb}} &= \dot{m} \left( h_e - h_i + \frac{v_e^2 - v_i^2}{2} \right) = \dot{m} (h_e - h_i + \Delta KE) \\
 &= \left( 12 \frac{\text{kg}}{\text{s}} \right) \left( 2875.5 \frac{\text{kJ}}{\text{kg}} - 2971.3 \frac{\text{kJ}}{\text{kg}} + 1.92 \frac{\text{kJ}}{\text{kg}} \right) \\
 &= 1126.56 \text{ kJ/s} \quad (1200 \text{ kW})
 \end{aligned}$$

## QUESTION DATA

### Vendor

0000087567

### Solving Time

### Difficulty

easy

### Quantitative?

No

### Status

Active

### Created On

07/11/2018 09:28:09 PM

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01/03/2020 08:32:49 PM

### OTHER VERSIONS

03/22/2016 08:52:45 PM

(/admin/questions/preview/91)

07/11/2018 09:28:09 PM

(/admin/questions/preview/111)

### DISCIPLINES

KNOWLEDGE AREAS

PRODUCTS USED IN

FECHPPW

FEMEPPW

## Chapter 29, Problem 4

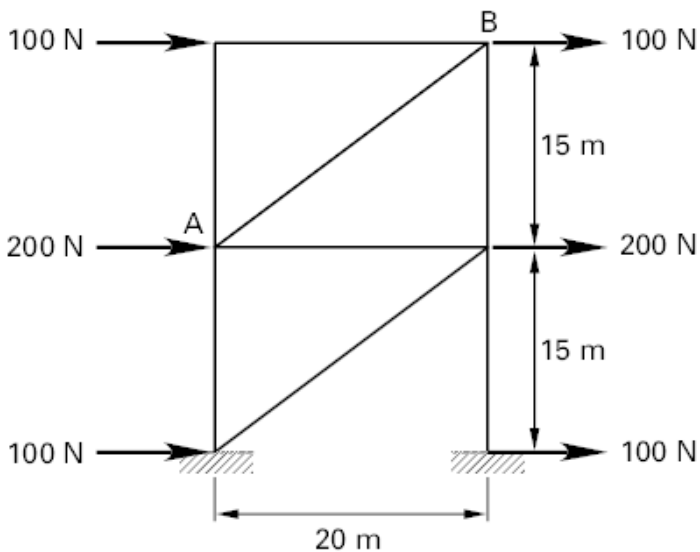
[Return to Questions \(/admin/questions/0?sfield=magento\\_id&stext=87724&sdka=&stype=&sdiff=\)](/admin/questions/0?sfield=magento_id&stext=87724&sdka=&stype=&sdiff=)

## Test Bank Question

preview

## Question

The braced frame shown is constructed with pin-connected members and supports. All applied forces are horizontal.



Most nearly, what is the force in the diagonal member BA?

## Answers

- (A) 0 N
- (B) 160 N
- (C) 200 N
- (D) 250 N

The answer is (D).

## Solution

Determine the length of member BA by recognizing this configuration to be a 3-4-5 triangle.

$$L_{BA} = 25 \text{ m}$$

Use the method of sections. Cut the frame horizontally through member BA.

## QUESTION DATA

## Vendor

0000087724

## Solving Time

2-4

## Difficulty

medium

## Quantitative?

Yes

## Status

Active

## Created On

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## OTHER VERSIONS

05/31/2017 06:41:25 P

(/admin/questions/prev

03/08/2018 07:35:49 P

(/admin/questions/prev

09/16/2019 07:14:57 P

(/admin/questions/prev

12/18/2019 08:07:07 P

(/admin/questions/prev

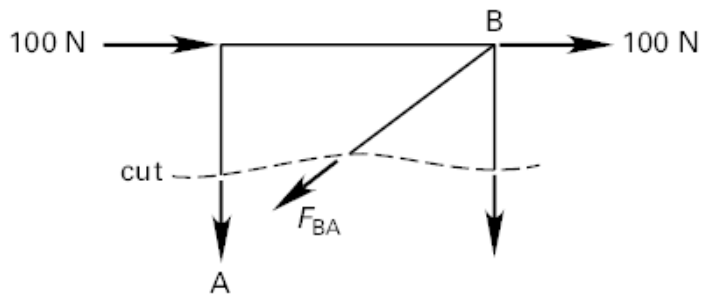
## DISCIPLINES

FE Civil

(/admin/questions/inde  
sfield=discipline&stext:  
Civil)

FE Mechanical

(/admin/questions/inde



By inspection, the horizontal component of  $F_{BA}$  balances the two applied horizontal loads.

$$BA_x = 100 \text{ N} + 100 \text{ N} = 200 \text{ N}$$

By similar triangles,

$$BA = \left( \frac{5}{4} \right) (200 \text{ M}) = 250 \text{ M}$$

sfield=discipline&stext:  
Mechanical)

FE Other Disciplines  
(/admin/questions/inde  
sfield=discipline&stext:  
Other Disciplines)

KNOWLEDGE AREAS

Statics  
(/admin/questions/inde  
sfield=area&stext=Stat

PRODUCTS USED IN

FEMEPPW

FECEPPW

FECHPPW

## Chapter 44, Problem 3

[Return to Questions \(/admin/questions/0?sfield=magento\\_id&stext=0000088708&sdka=&stype=&sdiff=\)](/admin/questions/0?sfield=magento_id&stext=0000088708&sdka=&stype=&sdiff=)

# Test Bank

Question preview

## Question

Aeration of a 500 m<sup>3</sup> wastewater pond is required as part of a bioremediation plan. Ten spargers located 4.6 m below the surface bubble compressed air through the pond at a rate of 0.425 m<sup>3</sup>/min each. The mass transfer provided by each sparger is given as a transfer factor (the overall liquid mass-transfer coefficient multiplied by the ratio of the average interfacial area of bubbles to volume of solution) equal to 0.0680 h<sup>-1</sup>. Most nearly, how long will it take to increase the water's dissolved oxygen concentration from 3 mg/L to 6 mg/L?

## Answers

- (A) 6.7 min
- (B) 40 min
- (C) 150 min
- (D) 390 min

The answer is (B).

## Solution

Mass transfer can be expressed in terms of the overall liquid mass-transfer coefficient,  $K_L$ . In this case,  $K_L$  is per sparger (not per sparger area), and since there is no well-defined sparger area, the variable  $A$  is interpreted as the number of spargers.

$$\frac{N_{O_2}}{A} = K_L (C_{O_2}^* - C_{O_2,L})$$

Expressed in differential form, the equation becomes

$$\frac{dN_{O_2}}{dt} = K_L A (C_{O_2}^* - C_{O_2,L})$$

Separating variables and integrating yields

## QUESTION DATA

### Vendor

0000088708

### Solving Time

2-4

### Difficulty

medium

### Quantitative?

Yes

### Status

Active

### Created On

10/04/2016 06:40:23 PM

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01/03/2020 08:33:13 PM

## OTHER VERSIONS

## DISCIPLINES

FE Other Disciplines

(/admin/questions/index?sfield=discipline&stext=FE Other Disciplines)

PE Mechanical: HVAC and Refrigeration

(/admin/questions/index?sfield=discipline&stext=PE

$$\int_{C_{O_2,L|0}}^{C_{O_2,L|t}} \frac{dC_{O_2,L}}{C_{O_2}^* - C_{O_2,L}} = K_L A \int_0^t dt$$

$$\ln \frac{C_{O_2}^* - C_{O_2,L|0}}{C_{O_2}^* - C_{O_2,L|t}} = K_L A t$$

$$t = \ln \frac{C_{O_2}^* - C_{O_2,L|0}}{C_{O_2}^* - C_{O_2,L|t}} \left( \frac{1}{K_L A} \right)$$

$$= \ln \frac{11.3 \frac{\text{mg}}{\text{L}} - 3.0 \frac{\text{mg}}{\text{L}}}{11.3 \frac{\text{mg}}{\text{L}} - 6.0 \frac{\text{mg}}{\text{L}}}$$

$$\times \left( \frac{1}{\left( \frac{0.0680}{\text{h} \cdot \text{sparger}} \right) (10 \text{ spargers})} \right) \left( 60 \frac{\text{min}}{\text{h}} \right)$$

$$= 39.6 \text{ min} \quad (40 \text{ min})$$

Mechanical: HVAC and Refrigeration)

PE Mechanical: Thermal and Fluid Systems  
(/admin/questions/index?sfield=discipline&stext=PE Mechanical: Thermal and Fluid Systems)

#### KNOWLEDGE AREAS

Thermodynamics and Heat Transfer (/admin/questions/index?sfield=area&stext=Thermodyn: and Heat Transfer)

Heat Transfer (/admin/questions/index?sfield=area&stext=Heat Transfer)

Heat Transfer Principles (/admin/questions/index?sfield=area&stext=Heat Transfer Principles)

PRODUCTS USED IN FECHPPW

## Chapter 46, Problem 1

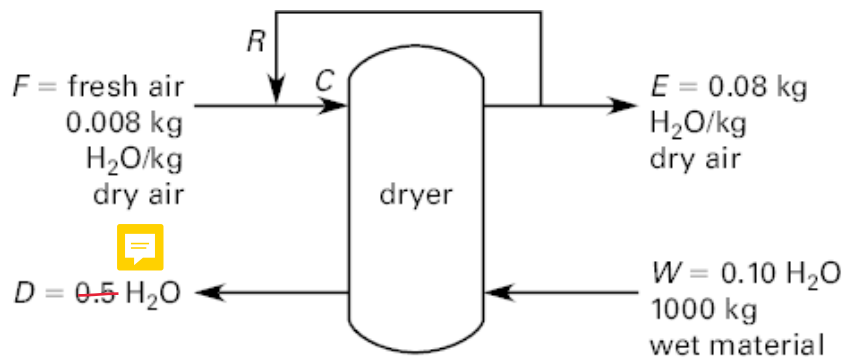
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# Test Bank

Question preview

## Question

A drying process with drying air recycle has a drying air inlet moisture mass fraction of 0.008 kg H<sub>2</sub>O/kg dry air and an outlet moisture mass fraction of 0.08 kg H<sub>2</sub>O/kg dry air. 1000 kg of moist material is introduced to the dryer. The material contains 10% (by mass) moisture and is to be dried to 5% (by mass) moisture. The mass fraction of moisture in stream *C* is 0.01 kg water/kg dry air. The dryer operates as shown. (*F*, *R*, *C*, *E*, *D*, and *W* represent individual streams.)



Most nearly, what is the total mass of stream *R*?

## Answers

- (A) 21 kg
- (B) 38 kg
- (C) 54 kg
- (D) 78 kg

The answer is (A).

## Solution

The overall mass balance of the system is

$$m_{\text{in}} = m_{\text{out}}$$

Complete a mass balance of the moist material, *W*. The mass of moist material out, *D*, is

## QUESTION DATA

### Vendor

0000088744

### Solving Time

### Difficulty

easy

### Quantitative?

No

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### OTHER VERSIONS

01/03/2020

08:33:14 PM

(/admin/questions/preview/12714)

### DISCIPLINES

KNOWLEDGE AREAS

PRODUCTS USED IN

FECHPPW

$$y_W W = y_D D$$

$$D = \frac{y_W W}{y_D}$$

$$(1 - 0.10)(1000 \text{ kg}) = (1 - 0.05)D$$

$$D = 947.5 \text{ kg}$$

The amount of water removed is

$$\begin{aligned} \text{water removed} &= W - D = 1000 \text{ kg} - 947.4 \text{ kg} \\ &= 52.6 \text{ kg} \end{aligned}$$

Perform an overall system total mass balance.

$$W + F = D + E$$

$$1000 \text{ kg} + F = 947.37 \text{ kg} + E$$

$$F - E = -52.63 \text{ kg}$$

Complete a water balance around the system.

$$x_W W + w_F F = x_D D + x_E E$$

$$(0.1)(1000 \text{ kg}) + \left(\frac{0.008}{1.008}\right)F = (0.5)(947.4 \text{ kg}) + \left(\frac{0.08}{1.08}\right)E$$

$$100 \text{ kg} + 0.0079F = 47.37 \text{ kg} + 0.074E$$

$$0.0079F - 0.074E = -52.63 \text{ kg}$$

Substitute the overall system balance equation.

$$0.0079(E - 52.63) - 0.074E = -52.63$$

$$0.0661E = 52.214 \text{ kg}$$

$$E = 789.9 \text{ kg}$$

$$F - E = F - 789.9 \text{ kg} = -52.63 \text{ kg}$$

$$F = 737.30 \text{ kg}$$

The mass of the dry air in the feed air is

$$\begin{aligned} z_F &= F \left(\frac{1}{1.008}\right) = (737.30 \text{ kg}) \left(\frac{1}{1.008}\right) \\ &= 731.45 \text{ kg} \end{aligned}$$

The mass balance around the point where the recycle loop joins the feed (i.e., where  $C$  is the flow into the dryer with the recycled and feed air) is

$$m_{W,F} + m_{W,R} = m_{W,C}$$

$$x_F F + x_R R = x_C C$$

Perform a water balance to find the mass of recycled air.

$$(731.45 \text{ kg}) \left( 0.008 \frac{\text{kg H}_2\text{O}}{\text{kg dry air}} \right)$$
$$+ R(0.08) = (731.45 \text{ kg} + R)(0.01)$$
$$5.85 \text{ kg} + 0.8R = 7.3145 \text{ kg} + 0.01R$$
$$\text{✉ } 0.07R = 1.465 \text{ kg}$$
$$R = 20.92 \text{ kg} \quad (21 \text{ kg})$$